

HENRI System in TREAT

Aaron Epiney

www.inl.gov



**International RELAP5-3D Users Group Meeting
December 4-8, 2023**

Overview

- Motivation for TREAT HENRI
- Description of the RELAP5-3D model
- Transient calculations
- Conclusions

Motivation for TREAT HENRI

TREAT – Overview

- The Transient Reactor Test (TREAT) facility resumed operations in order to support fuel safety testing and other areas of transient science.
- TREAT: Core comprised of air-blower-cooled, Zircaloy-clad graphite/fuel blocks.
 - 120 kW steady state, ~20 GW peak in pulse mode
 - Virtually any power history possible within 2500 MJ max core transient energy
 - No reactor pressure vessel/containment; facilitates access for in-core instrumentation

Experiment design

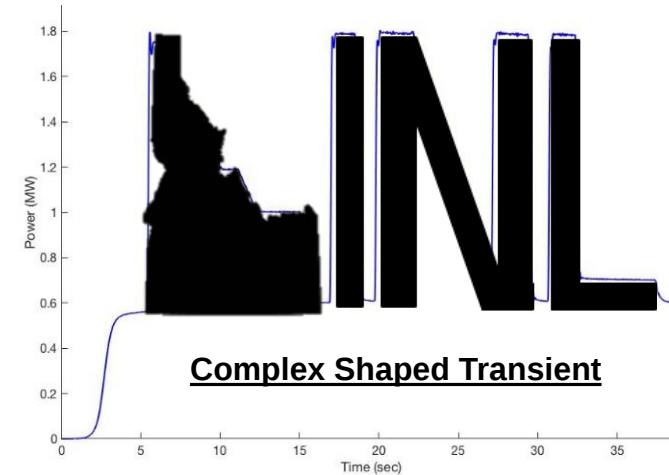
- The reactor provides neutrons, and the experiment vehicle does the rest
- The tests displace a few driver fuel assemblies, handled in a cask outside the core
- Recoverable historic designs do not include water-environment vehicles; new designs are needed

Four slots for viewing the core center

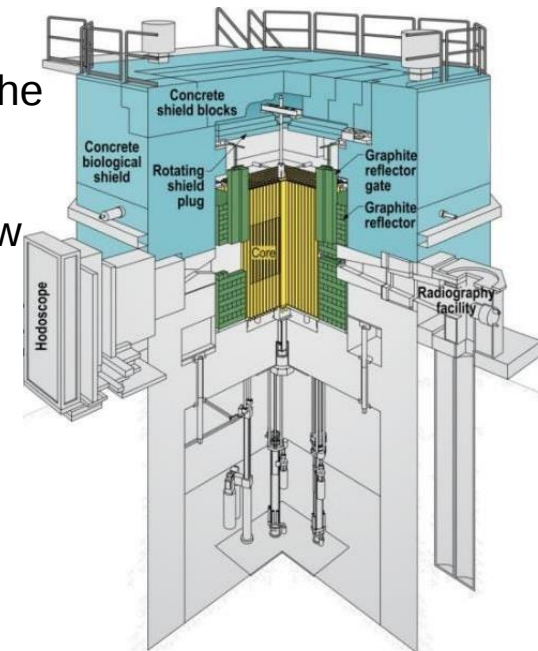
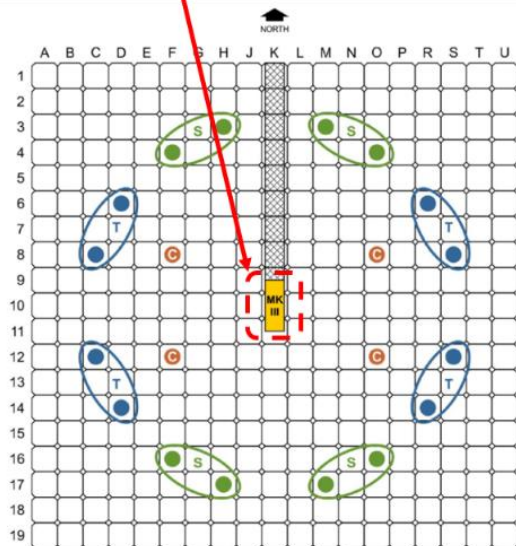
- Two are in use for the fast-neutron hodoscope, neutron radiography

Collocated with related facilities at INL

- ATR and HFEF
- Fuel fabrication and characterization



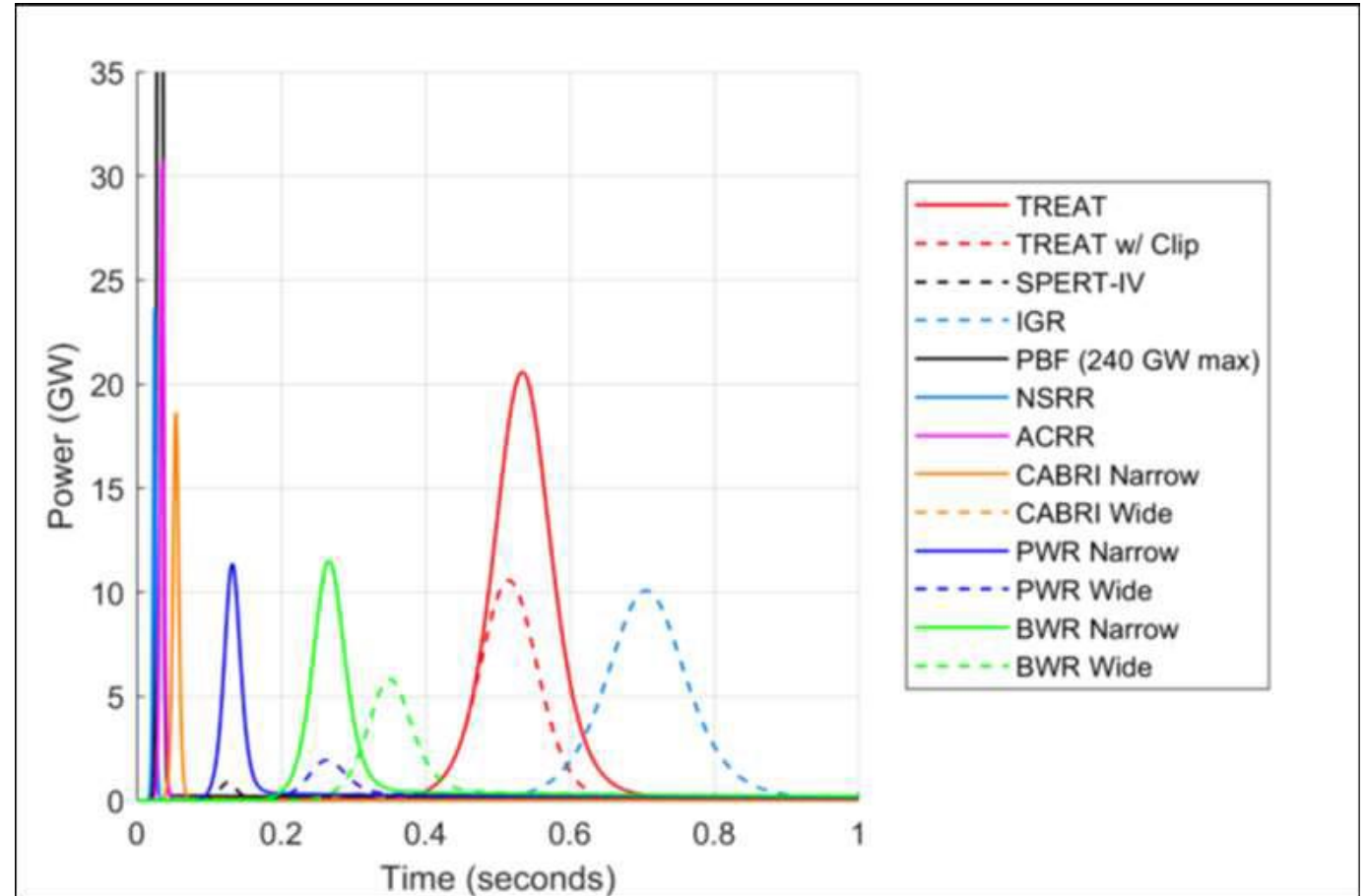
Typical Experiment Location



Advanced RIA testing at TREAT

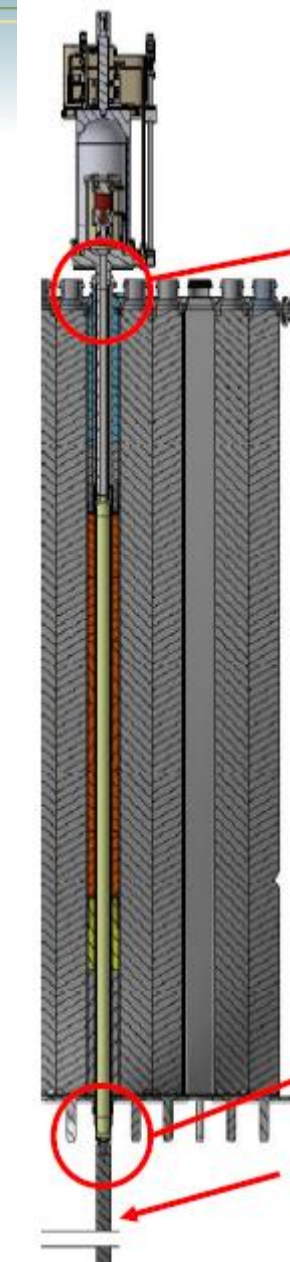
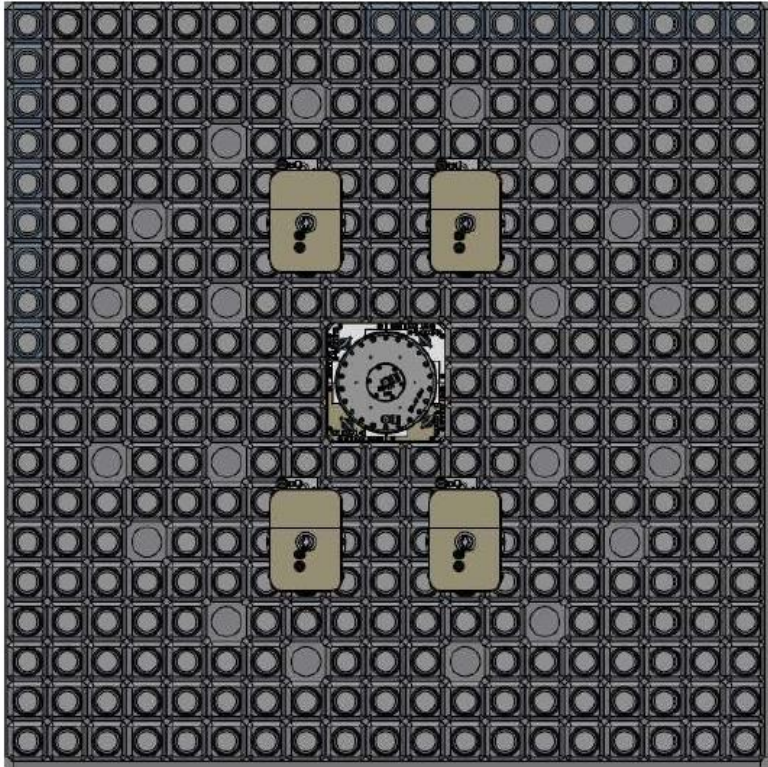
RIA testing for advanced nuclear fuel testing is desired, the problem being that no reactors are currently able to produce a sufficient “prototypic” pulse width for achieving the type of testing being modeled.

- Too wide or narrow pulse can lead to a non-prototypic reaction in the fuel.



HENRI

He³ Negative Reactivity Injection



Thermal-hydraulic design and safety considerations

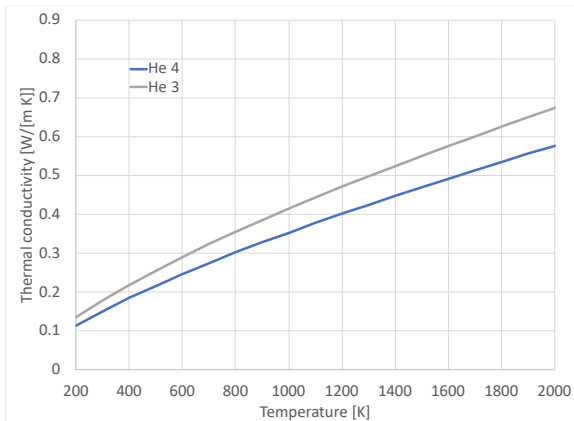
- There is an optimum He^3 loading balancing:
 - Negative reactivity insertion
 - Helium heating
- **Problem:** Find the worst-case scenario for the safety analysis
 - 4.5% dk/k step insertion. 1 HENRI already filled with He^3 . Can we get the reactor to start? This may be the case in which the most energy is deposited in the He^3 .
 - 4.5% dk/k step insertion. 1 HENRI fires at the pulse peak; the transient and other rods do not actuate until later.
 - 4.5% dk/k step insertion. HENRI does not fire until later, once the fuel assembly heat has led to the peak temperature.

HENRI TH model

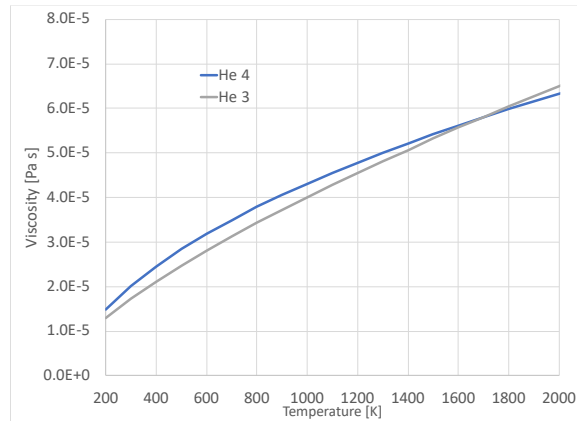
He³

He³ vs. He⁴ properties

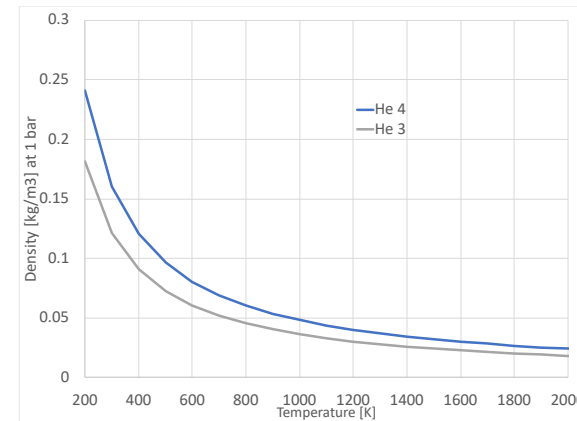
- The properties of He³ significantly differ from those of He⁴.
 - To properly capture helium heating (density) and pressure wave propagation (friction => viscosity), He³ properties were implemented in RELAP5-3D (as a new non-condensable option).



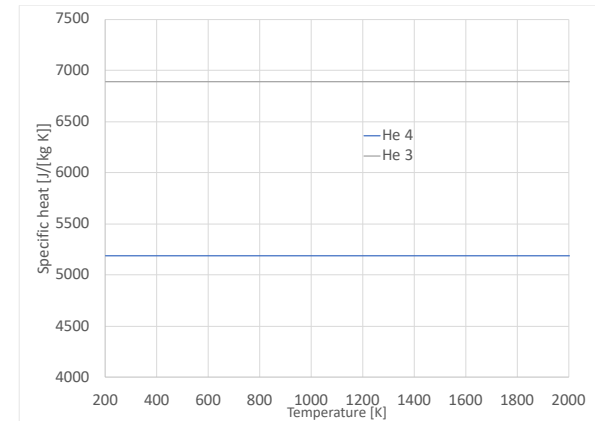
Thermal conductivity



Viscosity



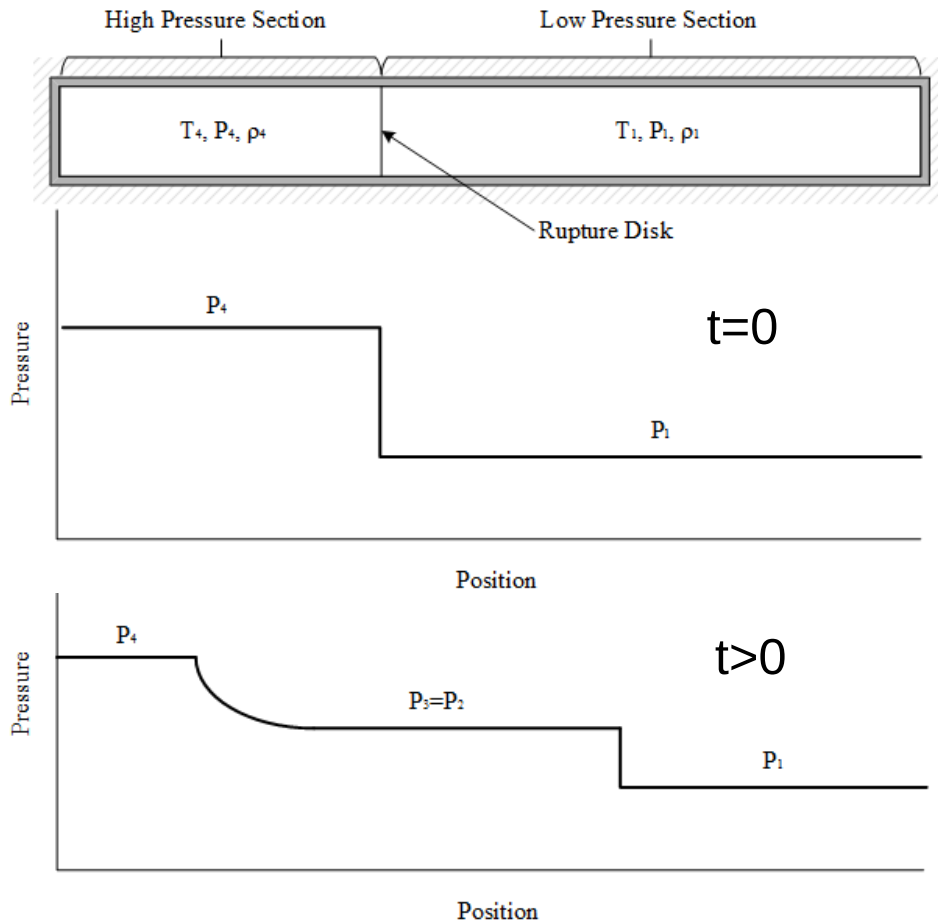
Density



Specific heat

Verification of the He^3 implementation in RELAP5-3D

- Shock tube analysis



Analytic solution

Pressure

$$\frac{P_4}{P_1} = \frac{P_2}{P_1} \left[1 - \frac{(\gamma - 1) \left(\frac{P_2}{P_1} - 1 \right)}{\sqrt{2\gamma \left[2\gamma + (\gamma + 1) \left(\frac{P_2}{P_1} - 1 \right) \right]}} \right]^{\frac{-2\gamma}{\gamma - 1}}$$

Temperature

$$\frac{T_2}{T_1} = \frac{P_2}{P_1} \left(\frac{\frac{\gamma+1}{\gamma-1} + \frac{P_2}{P_1}}{1 + \frac{(\gamma+1)P_2}{(\gamma-1)P_1}} \right)$$

Density

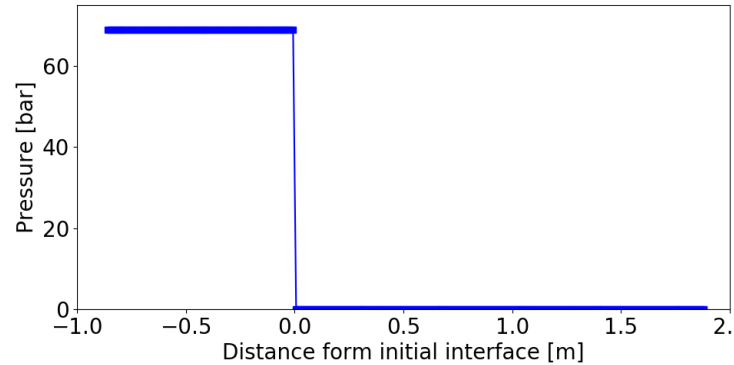
$$\frac{\rho_2}{\rho_1} = \frac{1 + \frac{(\gamma+1)P_2}{(\gamma-1)P_1}}{\frac{\gamma+1}{\gamma-1} + \frac{P_2}{P_1}}$$

Shock wave velocity

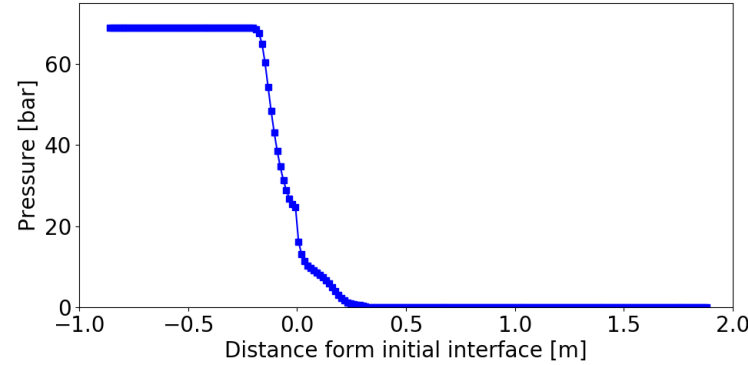
$$w = a \sqrt{\frac{\gamma + 1}{2\gamma} \left(\frac{P_2}{P_1} - 1 \right) + 1}$$

RELAP5-3D results

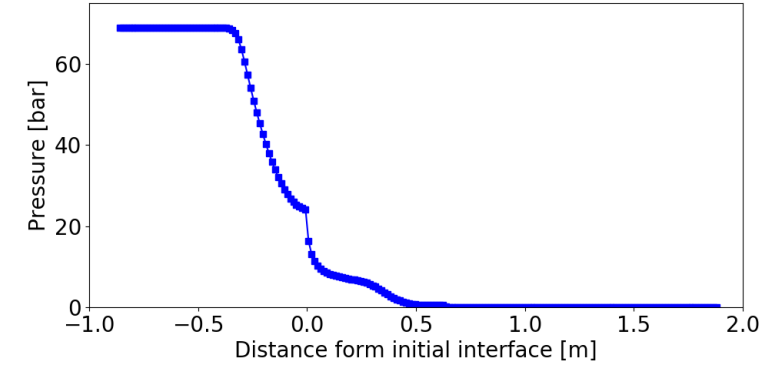
RELAP5-3D results for example pressure wave propagation in He3-filled shock tubes



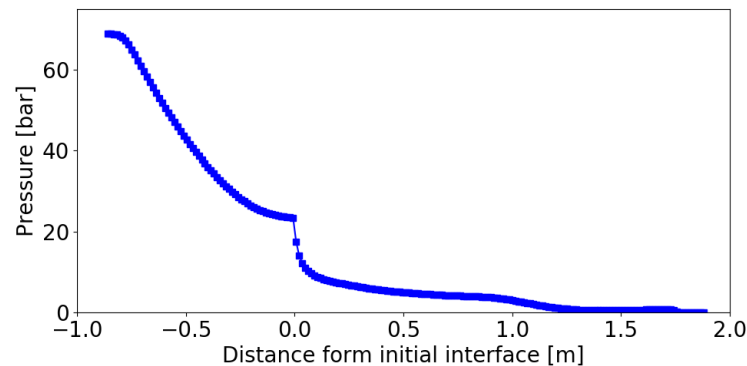
$t = 0.00$ ms



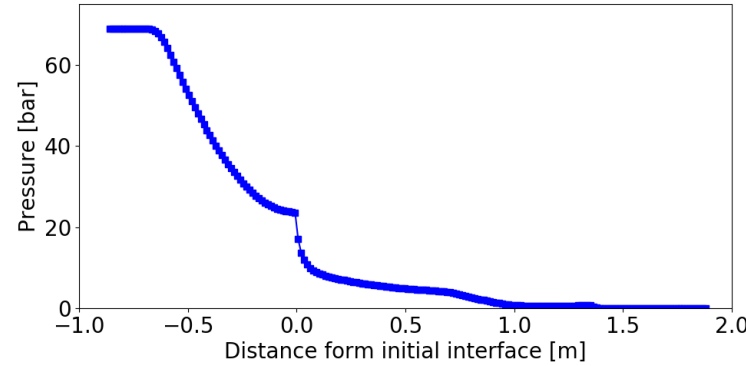
$t = 0.10$ ms



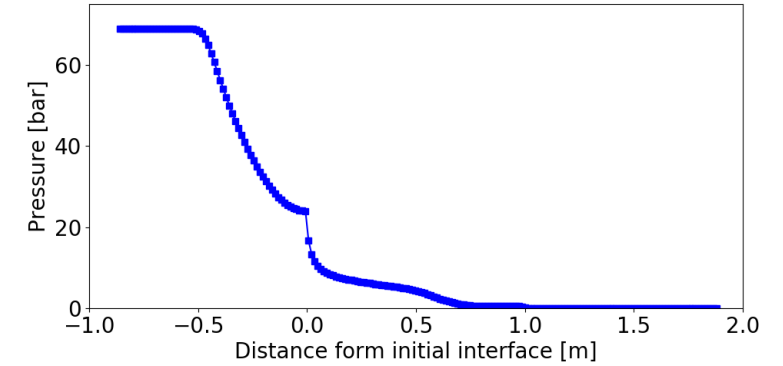
$t = 0.25$ ms



$t = 0.40$ ms



$t = 0.50$ ms



$t = 0.65$ ms

RELAP5-3D results vs. analytic solution

	RELAP5-3D		P4	P1	P2/P1			T2/T1			ρ_2/ρ_1			v [m/s]		
	Mesh size	Timestep	[bar] (psi)	[bar] (psi)	RELAP5	Theory	%	RELAP5	Theory	%	RELAP5	Theory	%	RELAP5	Theory	%
Mesh and timestep size	~1cm	1e-10 s	68.95 (1000)	0.0689 (1.0)	9.27	9.44	-1.74	2.96	3.27	-9.51	3.13	2.88	8.62	2687	2785	-3.52
	~1cm	1e-8 s	"	"	9.37	"	-0.71	2.98	"	-8.86	3.14	"	8.96	2697	"	-3.14
	~3cm	1e-8 s	"	"	8.40	"	-10.95	2.75	"	-15.74	3.04	"	5.71	2583	"	-7.25
	~6cm	1e-8 s	"	"	16.54	"	75.16	0.88	"	-73.09	18.77	"	550.86	238	"	-91.45
P4/P1 ratio	~1cm	1e-8 s	34.47 (500)	0.0689 (1.0)	8.13	8.32	-2.24	2.58	2.99	-13.54	3.14	2.78	13.04	2706	2619	3.33
	"	"	34.47 (500)	0.0344 (0.5)	8.48	9.44	-10.18	2.58	3.27	-20.96	3.27	2.88	13.62	2717	2785	-2.44
	"	"	34.47 (500)	0.0068 (0.1)	10.40	11.95	-12.89	2.07	3.90	-46.85	5.01	3.05	63.89	2710	3124	-13.25

As expected, higher P4/P1 ratios, and larger timesteps and mesh sizes make convergence more difficult.

The convergence study leads to guidelines for the safety analysis:

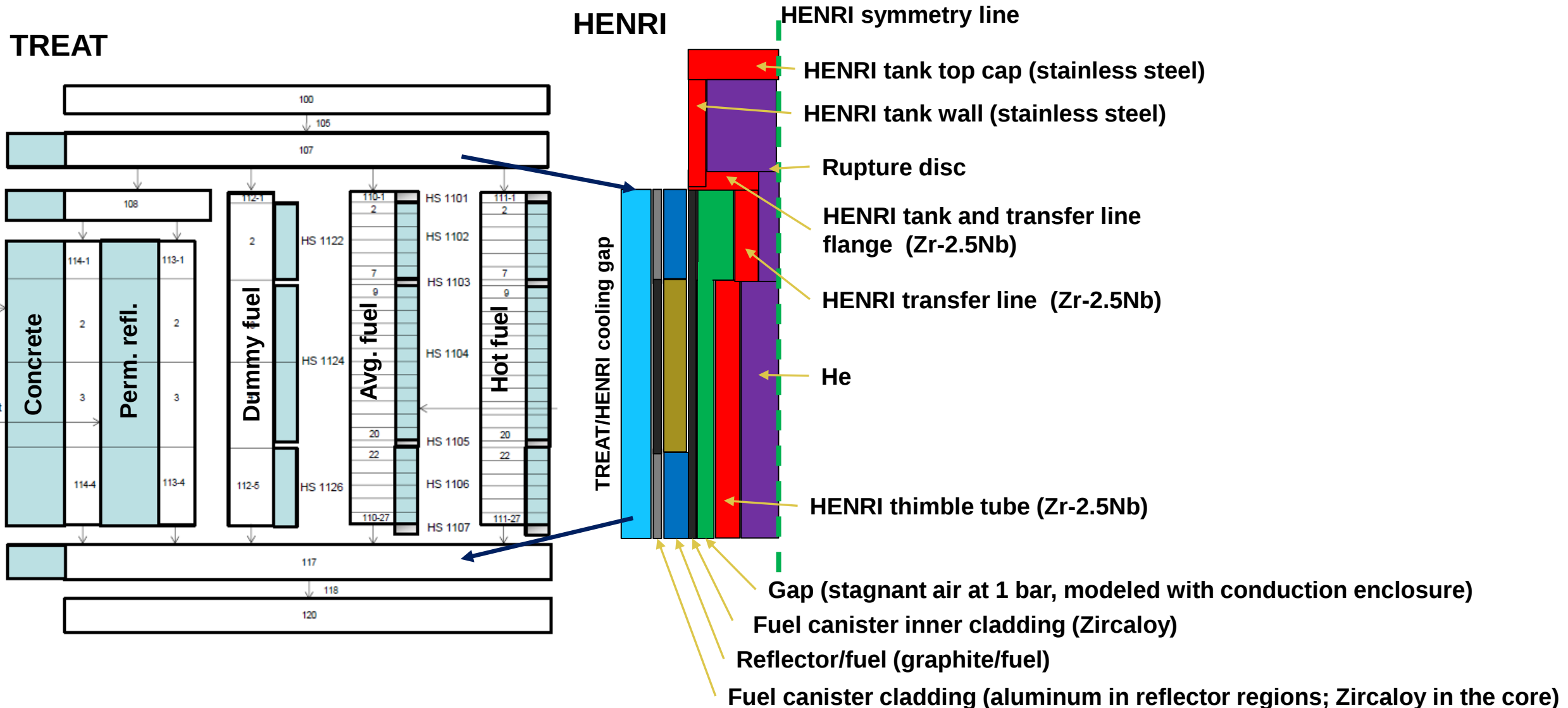
Acceptable results ($\pm 20\%$) and a still manageable computational time ($\sim 0.1x$ real-time [for the test problem]):

- P4/P1 ~ 1000
- Mesh size ~ 3 cm
- Timestep $\sim 1e-8$ s

HENRI TH model

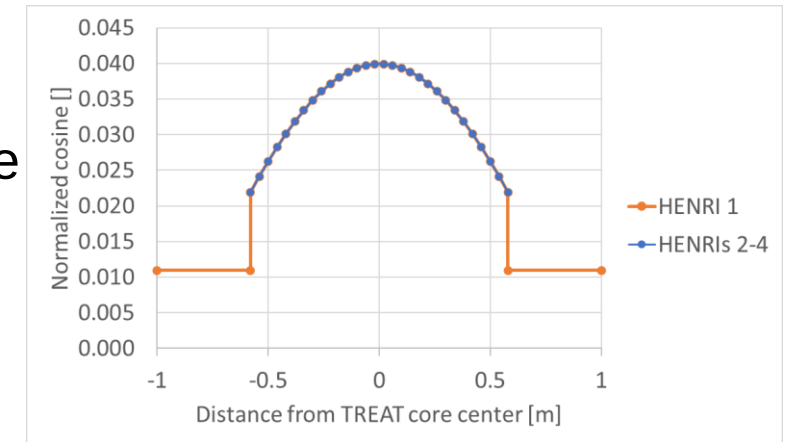
RELAP5-3D model

TREAT HENRI RELAP5-3D model (sketch not to scale!)



TREAT/HENRI RELAP5-3D model (general power model)

- Power is distributed in the **core and reflector regions** (for the HENRI with the highest PCFs).
- Axially, a chopped cosine with **axial peaking of 1.19** is assumed.
- Each HENRI has **individual heating rates** ([W/g]/MW_TREAT) for the **helium, HENRI tube, inner cladding, fuel, and outer cladding**.
- Provided heating rates are assumed at the core center.
- All materials are assumed to have the same axial shape (i.e., the distribution in the assembly is constant over the core length).
- No power is deposited in the stagnant air gap.

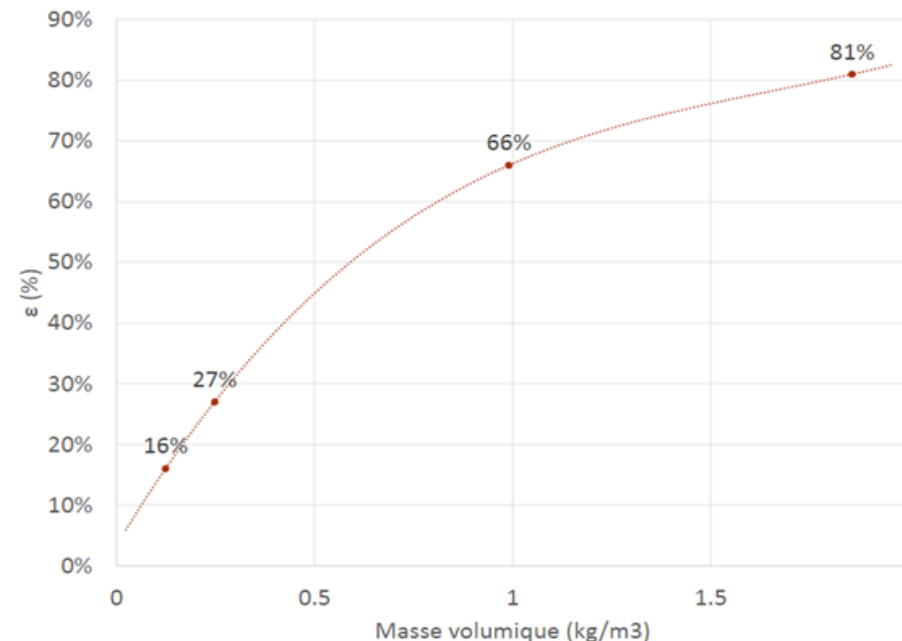


	Helium		HENRI tube		Inner cladding		Fuel		Outer cladding	
	250psi nom	250psi 1 HENRI	250psi	250psi 1 HENRI	250psi	250psi 1 HENRI	250psi	250psi 1 HENRI	250psi	250psi 1 HENRI
HENRI 1 upper refl	57.3	58	1.617E-03	1.593E-03	-	-	-	-	-	-
HENRI 1 core	290	283	4.951E-03	4.877E-03	6.751E-03	6.650E-03	1.760E-01	1.730E-01	1.293E-02	1.280E-02
HENRI 1 lower refl	66.8	65.8	1.617E-03	1.593E-03	-	-	-	-	-	-
HENRI 2	231	n/a	4.112E-03	n/a	5.559E-03	n/a	1.424E-01	n/a	1.050E-02	n/a
HENRI 3	280	n/a	4.781E-03	n/a	6.519E-03	n/a	1.699E-01	n/a	1.250E-02	n/a
HENRI 4	239	n/a	4.242E-03	n/a	5.737E-03	n/a	1.473E-01	n/a	1.086E-02	n/a

TREAT/HENRI RELAP5-3D model (He³ heating)

- **Helium heating:**

- The total helium mass in the core region was computed by RELAP5-3D.
- The total power deposited in the He was computed per the PCF (with the volume being averaged both radially and axially in the core) ([W/g]/MW_TREAT)
- A weighing factor was applied to account for the amount of heat absorbed by the gas, with the remaining energy going directly into the HENRI tube.
- The same axial shape used for the solids was applied.



TREAT/HENRI RELAP5-3D model (He³ reactivity feedback)

- The model is based on an existing TREAT point kinetic model using the M8 core kinetics and thermal feedbacks in the fuel
- Based on the provided data, the He³ reactivity was estimated as a function of helium density
- Six axial locations were evaluated via the neutronics calculations

$$He_{feedback}[\$] = M1[kg] * 291.7 \left[\frac{\$}{kg} \right] + M2[kg] * 3062.2 \left[\frac{\$}{kg} \right] + M3[kg] * 6075.2 \left[\frac{\$}{kg} \right] + M4[kg] * 5728.1 \left[\frac{\$}{kg} \right] + M5[kg] * 5000.7 \left[\frac{\$}{kg} \right] + M6[kg] * 1998.5 \left[\frac{\$}{kg} \right] + M7[kg] * 0.0 \left[\frac{\$}{kg} \right]$$

Transient Calculations

Identification of the overarching safety scenario

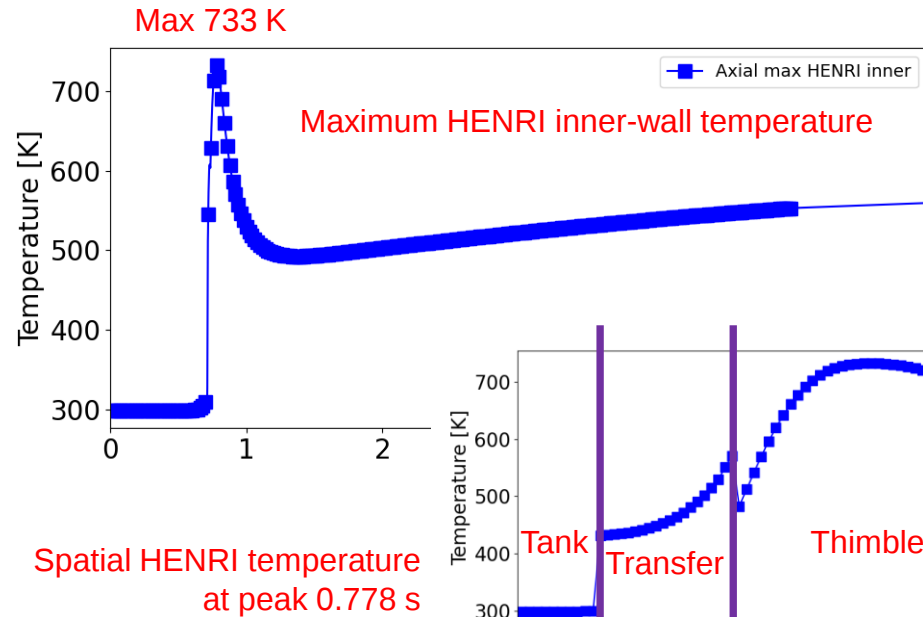
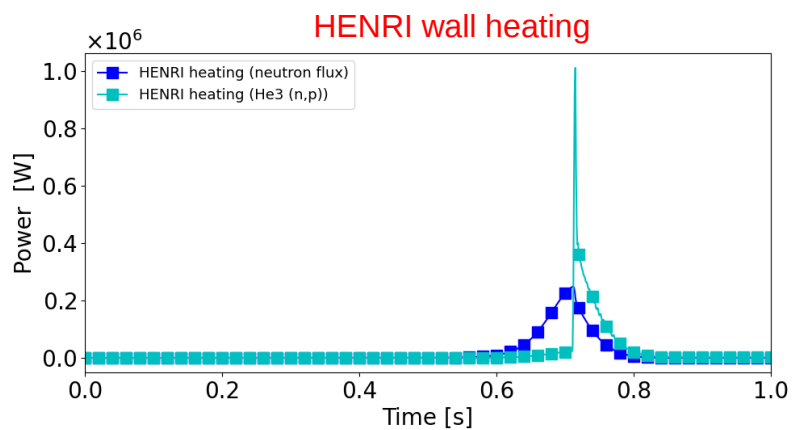
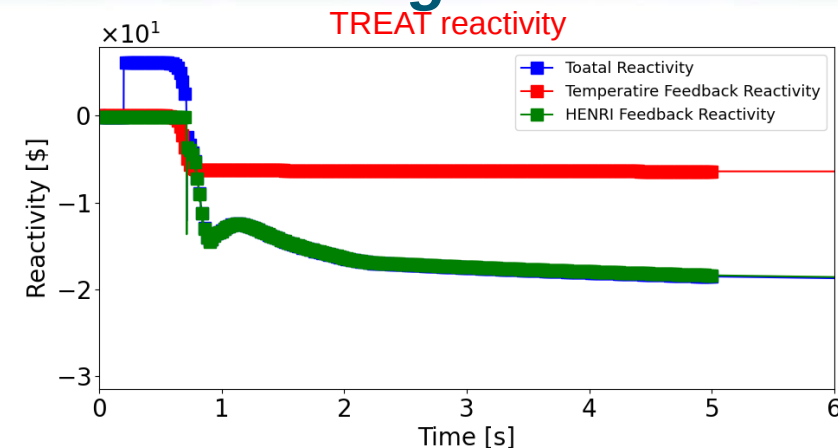
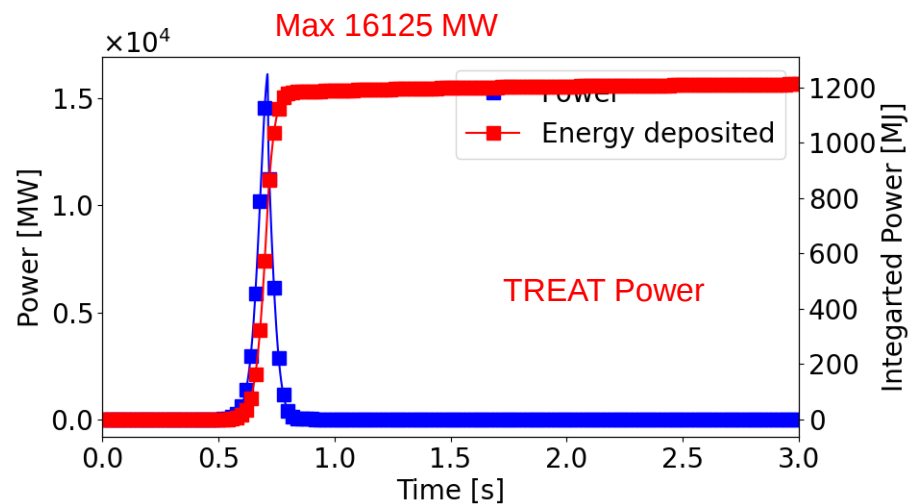
Transients investigated

- 4.5% dk/k reactivity insertion
- TREAT blowers running at a nominal 6000 CFM
- 250/400 psi (25°C) helium in tank
- 1" rupture disc opening in 1 ms
- Helium absorption reactivity and fuel temperature feedbacks considered; CRs re-inserted at 100 s (to avoid re-criticality)
- Scenarios
 - **Base calculation 1:** No HENRIs fire.
 - **Base calculation 2:** All 4 HENRIs fire at around the maximum power.
 - **Malfunction 1:** 1 HENRI fires 0.1 s before RIA insertion begins. 3 HENRIs fire normally
 - **Malfunction 2:** 1 HENRI fires on time, 3 HENRIs fire 1 s late.
 - **Malfunction 3:** 2 HENRIs fires on time, 2 HENRIs fire 1 s late.
 - **Malfunction 4:** 3 HENRIs fires on time, 1 HENRI fires 1 s late.

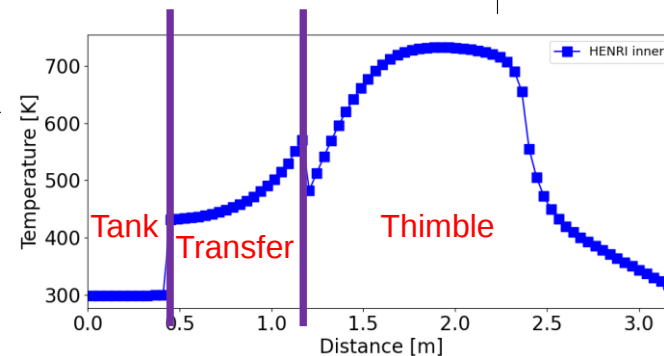
Sensitivities

- HENRI fire time: 0.6 s, max power @ 0.71 s, and 0.8 s
- Location of HENRI transfer line to the thimble connection: (1) nominal length and (2) 56.5 cm higher in the core reflector
- Initial tank pressures
 - Page 31 of Silvino A. Balderrama Prieto's master's thesis identifies 200 PSI as the minimum pressure for reaching the He^3 density necessary to generate the negative reactivity needed to clip the peak to <5 ms.
 - 250 and 400 PSI

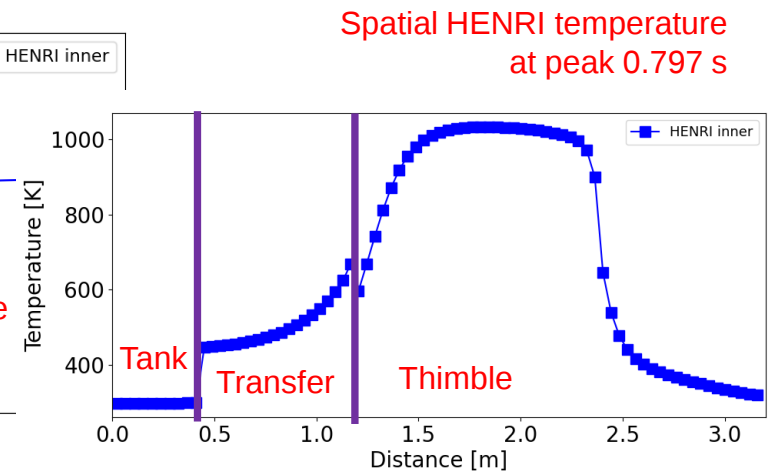
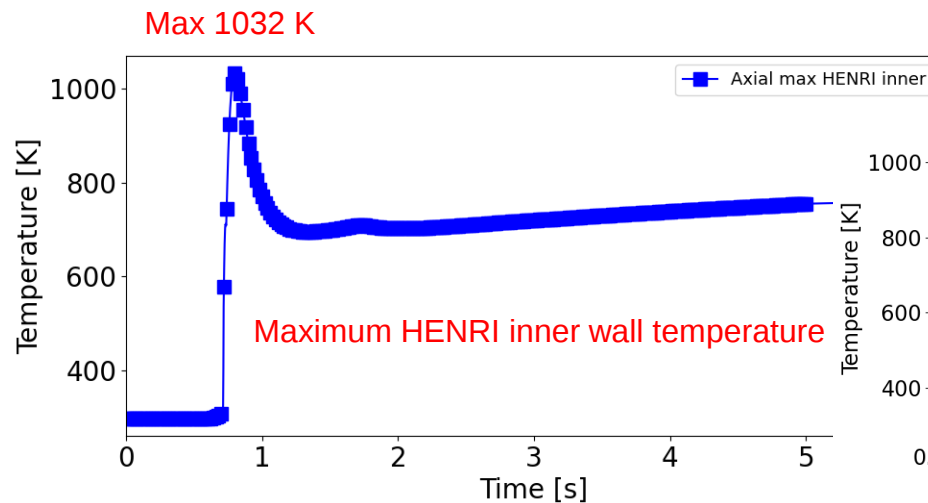
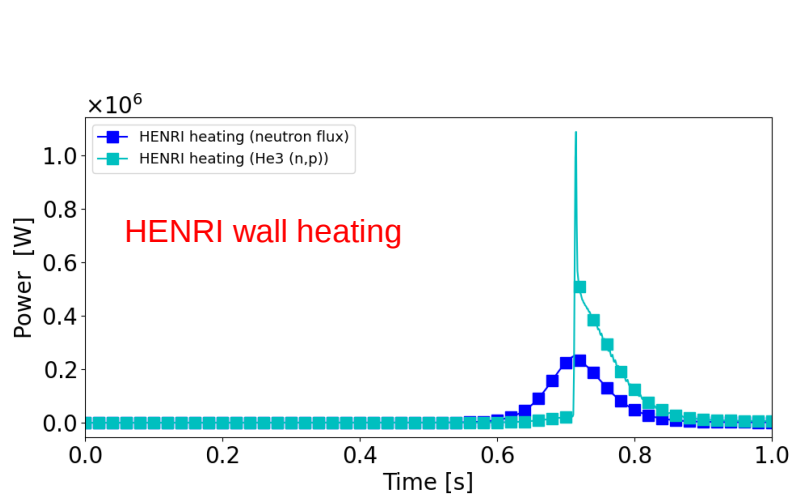
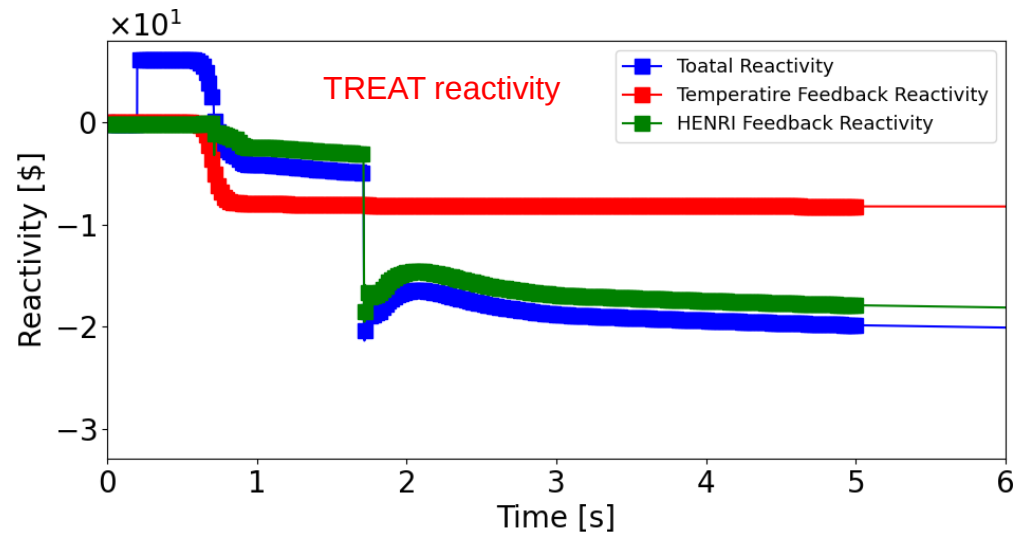
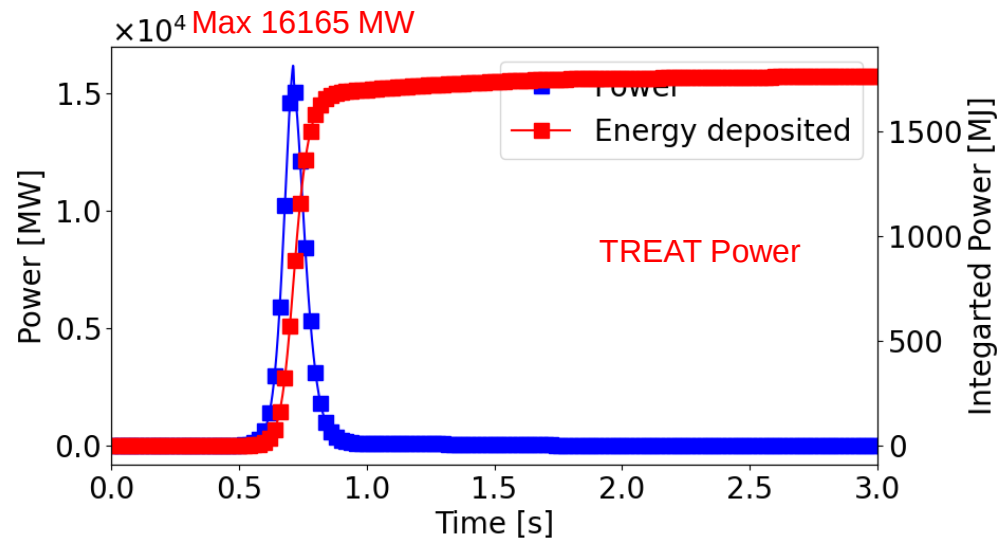
Nominal case: All 4 HENRIs fire at the peak, 250 PSI initial loading



Spatial HENRI temperature at peak 0.778 s



Malfunction 2: 1 HENRI fires normally (0.71 s) (250 PSI) 3 HENRIs fire late (1.71 s)



Summary

Sensitivity	TREAT max power [MW]	TREAT integrated power [MJ]	Max temp [K]
Base calc 1: No HENRIs fire	17330	2100	763
Base calc 2: 4HENRIS at max peak	16125	1200	705
Base calc 2: More tank pressure	16092	1100	829
Base calc 2: Shorter transfer line	16140	1250	641
Base calc 2: More tank pressure & shorter transfer line	16108	1150	718
Base calc 2: 4 HENRIES early 0.1 second	702	27	372
Base calc 2: 4 HENRIES early 0.1 second: More tank pressure	692	25	400
Base calc 2: 4 HENRIES late 0.1 second	16555	1900	716
Base calc 2: 4 HENRIES late 0.1 second: More tank pressure	16555	1900	783
Malf 1: 1 HENRI before RIA starts	0	0	300
Malf 1: 1 HENRI before RIA starts: More tank pressure	0	0	300
Malf 2: 1 HENRI at max, 3 late	16165	1750	954
Malf 2: 1 HENRI at max, 3 late: More tank pressure	16157	1700	1258
Malf 2: 1 HENRI at max, 3 late: Shorter transfer line	16185	1750	883
Malf 2: 1 HENRI at max, 3 late: More tank pressure & shorter transfer line	16173	1700	1063
Malf 3: 2 HENRIs at max, 2 late	16151	1500	860
Malf 3: 2 HENRIs at max, 2 late: More tank pressure	16134	1400	1012
Malf 4: 3 HENRIs at max, 1 late	16138	1300	744
Malf 4: 3 HENRIs at max, 1 late: More tank pressure	16114	1200	950

Conclusions

- **250 PSI:**
 - 4 HENRIs at peak 705 K
 - 3 HENRIs at peak 744 K
 - 2 HENRIs at peak 860 K
 - 1 HENRI at peak 954 K

The worst-case scenario is 1 HENRI firing at peak and 3 firing late
- **400 PSI**
 - 4 HENRIs at peak 829 K
 - 3 HENRIs at peak 950 K
 - 2 HENRIs at peak 1012 K
 - 1 HENRI at peak 1258 K

More tank pressure leads to higher max HENRI temperatures
- **Sensitivity:** All HENRIs fire early or late (within 0.1 s of the peak)
 - HENRIS fire early -> significantly less power deposited -> temperatures stay low
 - HENRIS fire late -> the amount of power deposited approaches case in which no HENRIs fire -> temperatures are the same as for the case in which no HENRIS fire
- **HENRI fires before RIA begins**
 - **TREAT remains subcritical**
- **Shorter transfer line**
 - The amount of power deposited slightly increases and the HENRI temperature slightly decreases.
 - No change in the axial location of max temperature.

The same effect as lowering the tank pressure
- Use the minimum amount of pressure needed to reach the target peak width.
- The worst-case scenario was when 1 HENRI fired at peak power -> 954 K for 250 PSI, and 1258 K for 400 PSI.
- Shortening the transfer line has the same effect as lowering the tank pressure.



Idaho National Laboratory