



Six-Field Model and RELAP5-3D

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Outline

- Six Field Equations
- Data to match
- Solution Algorithm
- RELAP Model
- Changes to Code
- Results
- References



Motivation for Six-Field Model

- Two-field models
 - Limited capability to model reactor transients and accidents
 - Cannot capture differences in temperature between liquid and droplet fields
 - Cannot track location of droplets or bubbles
- Six-field models
 - Improved accuracy of the calculations
 - Better accuracy will improve efficiency of nuclear reactor systems



Six Field Nomenclature

Index	Description
1	Continuous Liquid
2	Large Droplet
3	Small Droplet
4	Continuous Vapor
5	Large Bubble
6	Small Bubble

- Subscripts on terms in governing equations will indicate which field relates to that term
- Terms that refer to transition between fields (e.g., droplet entrainment, large droplets breaking into small droplets), two subscripts are provided.
 - The first subscript is the source field
 - The second subscript will indicate the result field (e.g. $S_{2,3}$).



Droplet Field Entrainment in RELAP5-3D

- First step in six-field implementation
- Single droplet field (small droplets) modeled
- Graded approach allows for confirmatory calculations before proceeding
- Entrainment correlation is added to vexplt
 - Computes rate of droplet entrainment based on local conditions in each control volume
 - Droplets not convected to other volumes
 - Droplets “disappear” each timestep



MASS (Continuity) Balance Governing Equations

- Continuous Liquid

$$\bullet \frac{\partial}{\partial t} (\alpha_1 \rho_f) + \nabla \cdot (\alpha_1 \rho_f \vec{v}_1) = -\Gamma_1 - \textit{Sink} + \textit{Source}$$

- Droplet Field

$$\bullet \frac{\partial}{\partial t} (\alpha_3 \rho_f) + \nabla \cdot (\alpha_3 \rho_f \vec{v}_3) = -\Gamma_3 - \textit{Sink} + \textit{Source}$$

- Continuous Vapor

$$\bullet \frac{\partial}{\partial t} (\alpha_4 \rho_g) + \nabla \cdot (\alpha_4 \rho_g \vec{v}_4) = -\Gamma_4 - \textit{Sink} + \textit{Source}$$



MOMENTUM Governing Equations

- Continuous liquid field

$$\alpha_1 \rho_f \frac{D\vec{v}_1}{Dt} = -\alpha_1 \nabla p_f + \alpha_1 \rho_f \vec{g}_1 + (\vec{v}_{i,1} - \vec{v}_1) \Gamma_1 + M_{i,1} + M_{w,1} - Sink + Source$$

- Droplet field

$$\alpha_3 \rho_f \frac{D\vec{v}_3}{Dt} = -\alpha_3 \nabla p_f + \alpha_3 \rho_1 \vec{g}_3 + (\vec{v}_{i,3} - \vec{v}_3) \Gamma_3 + M_{i,3} - Sink + Source$$

- Continuous vapor field

$$\alpha_4 \rho_g \frac{D\vec{v}_4}{Dt} = -\alpha_4 \nabla p_g + \alpha_4 \rho_g \vec{g}_4 + (\vec{v}_{i,4} - \vec{v}_4) \Gamma_4 + (\vec{v}_{i,3} - \vec{v}_4) \Gamma_3 + M_{i,4} + M_{w,4} - Sink + Source$$

Where:

\vec{g} – Body force (i.e., gravity)

\vec{v} – Velocity of the field (subscript i indicates near the interface)

$M_{i,1}$ – Momentum source from interfacial drag between continuous liquid and continuous vapor

$M_{w,1}$ – Momentum source from interfacial drag between continuous liquid and the wall

ENERGY Governing Equations

- Continuous liquid

- $$\alpha_1 \rho_f \frac{Dh_1}{Dt} = \alpha_1 \frac{Dp_f}{Dt} + \Phi_1^T + \Phi_1^\mu + \Gamma_{i,1}(h_{i,1} - h_1) + \Gamma_{w,1}(h_{w,1} - h_1) + a_i q_{i,1}''' + a_{w,1} q_{w,1}''' + M_{i,1}(\vec{v}_{i,1} + \vec{v}_1) - Sink + Source$$

- Droplet field

- $$\alpha_3 \rho_f \frac{Dh_3}{Dt} = \Gamma_{i,3}(h_{i,3} - h_3) + a_i q_{i,3}''' + M_{i,3}(\vec{v}_{i,3} + \vec{v}_3) - Sink + Source$$

- Continuous vapor

- $$\alpha_4 \rho_g \frac{Dh_4}{Dt} = \alpha_4 \frac{Dp_g}{Dt} + \Phi_4^T + \Phi_4^\mu + \Gamma_{i,4}(h_{i,4} - h_4) + \Gamma_{w,4}(h_{w,4} - h_4) + \Gamma_{i,3-4}(h_{4,3} - h_4) + a_i q_{i,4}''' + a_{4,3} q_{4,3}''' + a_{w,4} q_{w,4}''' + M_{i,4}(\vec{v}_{i,4} + \vec{v}_4) - Sink + Source$$

Where:

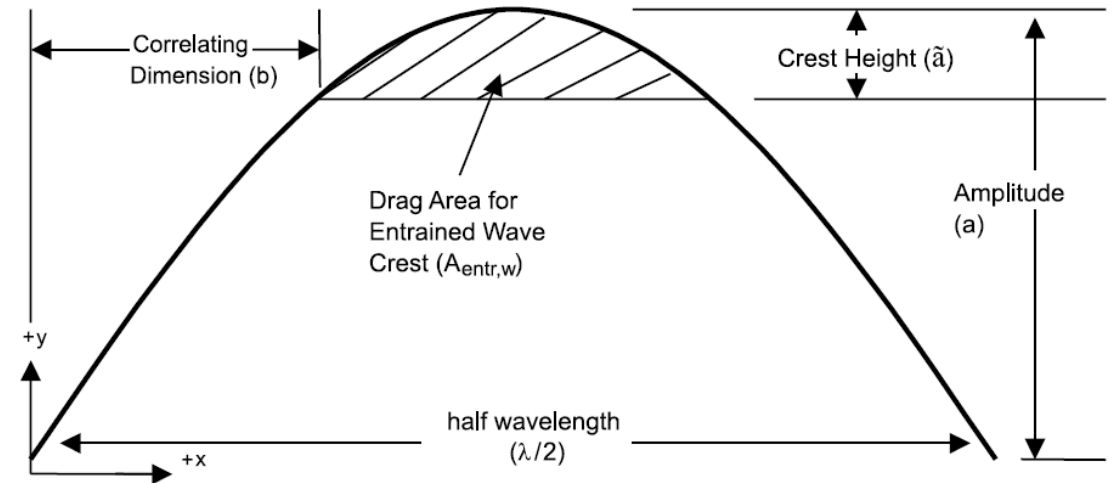
Φ – Viscous dissipation (superscript m) or turbulent work effect (superscript T)

h – Enthalpy (subscript i indicates interface)

a – interfacial area concentration (area per unit volume) at the w -wall or i -interface

q''' – Heat flow to continuous liquid from the w -wall or i -interface to the field

- Three primary entrainment mechanisms
 - Reflood – droplets entrained by flashing vapor
 - Vertical annular flows – droplets entrained from wave formation
 - Horizontal annular flows – droplets entrained from wave formation
- Annular wave entrainment
 - Wavelets form on annular flow surface from shear with vapor flow
 - Tops of wavelets pulled by shear forces
 - Sufficient shear overcomes surface tension, and droplets are entrained





Droplet Entrainment

- Source of mass to droplet field
- Sink of mass from the continuous liquid field
- Droplet entrainment model

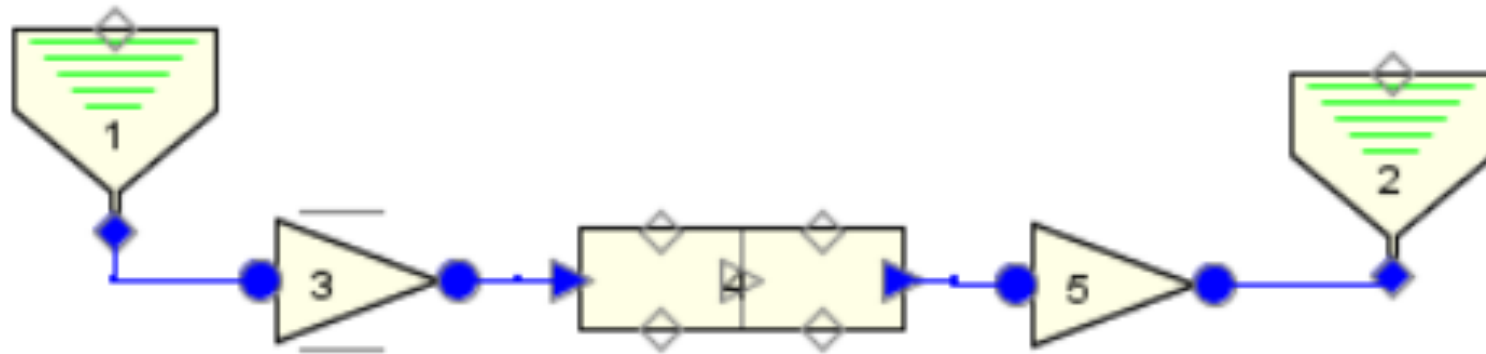
$$S_{1,3}''' = \frac{k'_A U_g^2 (\rho_g \rho_f)^{1/2} (W_{film} - W_{LFC})}{p \sigma t_{film}}$$



Entrainment Model Implementation in RELAP5-3D

- Two data structures added
 - Contain droplet-specific values for junctions and volumes
- Immediately prior to call to vexplt in the hydro module, droplet specific values are updated with liquid field parameters
 - Limits entrainment results to a single timestep

- Simple case that allows for 2-phase flow with control of the vapor and liquid velocities
- Two-volume PIPE connected to source and sink TDVs
- Inlet controlled by TDJ, outlet is a single junction



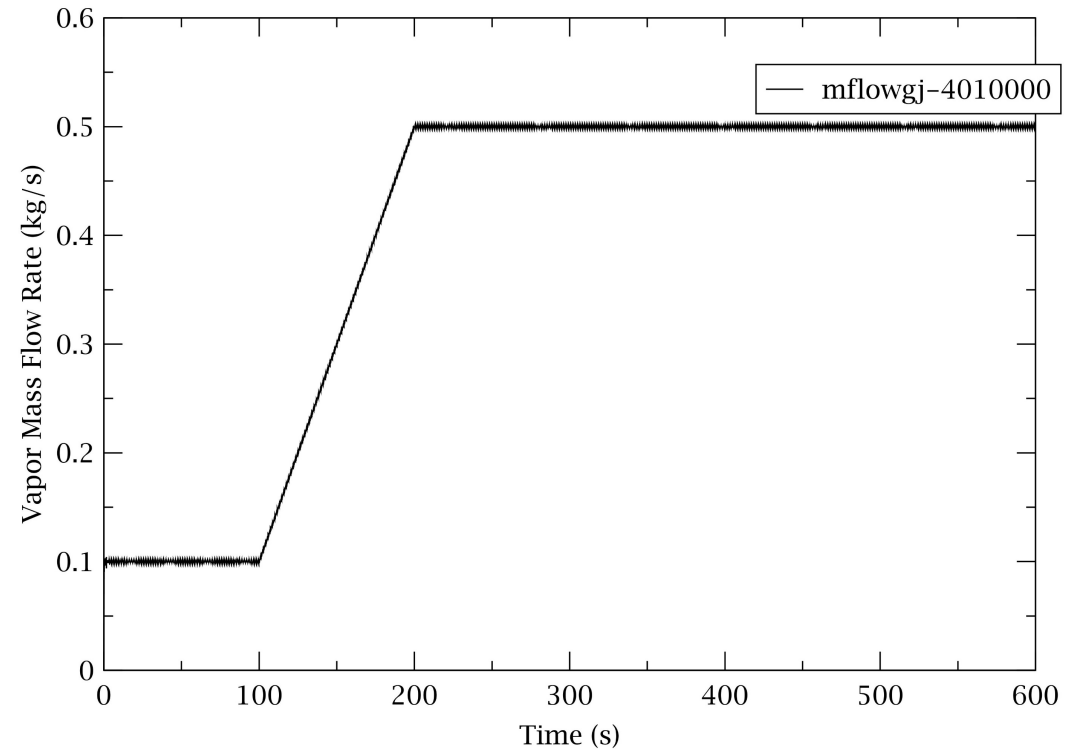
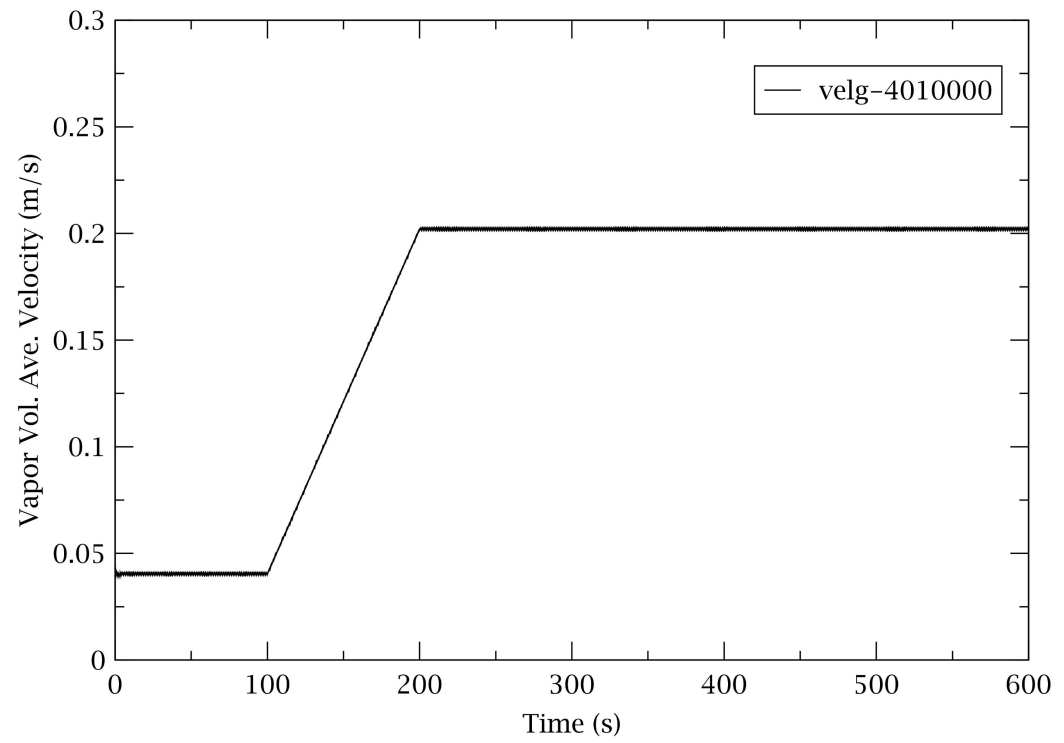


Test Case Conditions

- Inlet conditions
 - $T = 422.0 \text{ K}$
 - $X = 0.9$
 - $M_{\text{flowg}} = 0.1 \text{ kg/s} \rightarrow 0.5 \text{ kg/s}$
 - $M_{\text{flowf}} = 10 \text{ kg/s}$
- Test section PIPE
 - $FA = 1.0 \text{ m}^2$
 - $L = 2.0 \text{ m}$ (each volume)
 - $V = 2.0 \text{ m}^3$ (each volume)



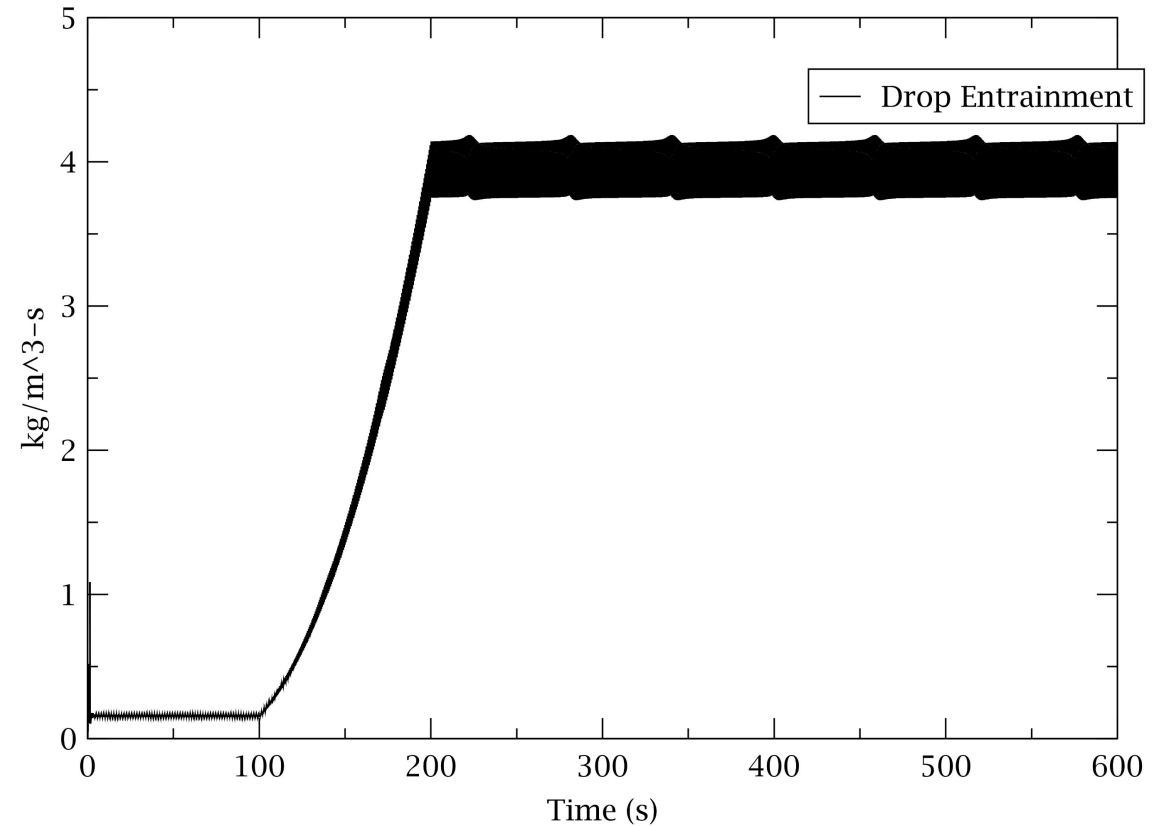
Test Section Vapor Flows





Droplet Entrainment Rate

- Volume of each PIPE cell is 2 m³
- Liquid fractions as high as 0.0003
- Droplet entrainment peaks at ~4 kg/m³-s
- Approximately 0.0024 kg of droplets entrained every second





References

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- L. Pan, T. J. Hanratty, “Correlation of entrainment for annular flow in horizontal pipes”, *International Journal of Multiphase Flow*, 28 385–408 (2002).
- G. A. Roth, G. Mesina, F. Aydogan, “Solving the six-field governing equations for a system code”, *Annals of Nuclear Energy*, 122, 366–377 (2018).